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**THE FOLLOWING IS THE ENGLISH TRANSLATION OF THE
ARTICLE 34 AMENDED SHEETS (Pages 32 and 33)**

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We claim:

1. A process for preparing polyisocyanates by reacting organic amines with phosgene, wherein the reaction is carried out in at least three stages, with the first stage being carried out in a mixing apparatus, the second stage in at least one residence apparatus and the third stage in one or more (reaction) columns and the pressure in each successive stage being lower than that in the previous stage.
2. A process as claimed in claim 1, wherein the polyisocyanate is diphenylmethane diisocyanate (MDI), polyphenylene-polymethylene polyisocyanate (PMDI) or a mixture of these two, tolylene diisocyanate (TDI), hexamethylene diisocyanate (HDI) or isophorone diisocyanate (IPDI).
3. A process as claimed in claim 1, wherein a nozzle is used as apparatus for the first stage.
4. A process as claimed in claim 1, wherein a tube reactor, a stirred vessel, an unstirred residence apparatus or a phase separation apparatus for gas and liquid phases is used as apparatus for the second stage.
5. A process as claimed in any of claims 1-4, wherein the residence time in the residence apparatus of the second stage is from 1 second to 30 minutes, preferably from 30 seconds to 10 minutes, particularly preferably from 2 to 7 minutes.
6. A process as claimed in any of claims 1-5, wherein the residence reactor of the second stage is configured as two or more reactors of the same or different types which are connected in parallel or in series.
7. A process as claimed in claim 1, wherein the phosgene is separated off in the apparatus of the third stage, preferably a (reaction) column.
8. A process as claimed in claim 1, wherein the pressure is reduced from the pressure of the reactor of the first stage to the pressure of the reactor of the second stage by means of a regulating valve or some other device characterized by a pressure drop.

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9. A process as claimed in claim 1, wherein the pressure is reduced from the pressure of the reactor of the second stage to the pressure of the reactor of the third stage by means of a regulating valve or some other device characterized by a 5 pressure drop.
10. A process as claimed in claim 1, wherein the reactor of the first stage is integrated into the reactor of the second stage.
10. A process as claimed in any of claims 1 to 9, wherein the pressure upstream of the static mixer is 3-70 bar, preferably 15-45 bar, the pressure in the reactor of the second stage is 2.5-35 bar, preferably 15-35 bar, and the pressure in the 15 reactor of the third stage is 2-20 bar, preferably 3.5-16 bar.
20. A process as claimed in any of claims 1 to 10, wherein the temperature in the first, second and third stages is in each case 80-190°C, preferably 90-150°C.
25. A process as claimed in any of claims 1 to 11, wherein an aromatic hydrocarbon such as toluene or preferably a chlorinated aromatic hydrocarbon such as chlorobenzene, ortho-dichlorobenzene or trichlorobenzene or a mixture thereof is used as inert solvent.

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